



Sensitivity Analysis of an Optimal Control Problem in Greenhouse Climate Management

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Optimal control systems are based on a performance measure to be optimised and a model description of the dynamic process to be controlled. When on-line implementation is considered, the performance of optimally controlled processes will depend on the accuracy of the model description used. Sensitivity analysis offers insight into the impact of uncertainty in the model parameters on the performance of the optimally controlled process. Additionally, sensitivity analysis may reveal the mechanisms underlying optimal process operation. This paper describes the methodology and results of a sensitivity analysis of an optimal control problem in greenhouse climate management. The methodology used, is based on variational arguments and requires a single solution of the optimal control problem, resulting in a computationally efficient technique. The example considered deals with economic optimal greenhouse climate management during the cultivation of a lettuce crop. The sensitivity analysis produced valuable insight into the performance sensitivity and operation of the controlled process. Both the model description of crop growth and production as well as the outside climate conditions have a strong impact on the performance. Humidity control plays a dominant role in economic optimal greenhouse climate management, emphasising the need for an accurate description of humidity effects on crop growth and production, either in terms of quantitative models or time-varying constraints on the humidity level in the greenhouse. Finally, the study revealed that the dynamic response times in the greenhouse climate are not limiting factors for economic optimal greenhouse climate control.

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1. Introduction

The optimal control methodology is a powerful technique to facilitate the design and analysis of optimally controlled systems. Optimal control systems are based on a model description of the dynamic process to be controlled and are designed in such a way that a performance criterion is optimised with respect to the control action applied to the system (*e.g.* Pontryagin *et al.*, 1962). In practice, the structure as well as the parameter values of the model rarely coincide exactly with the real process. Since the control system is designed to be optimal with particular regard to the nominal structure and parameter values of the model used, it can be expected that the control system is sensitive to modelling errors which may reduce the performance of an optimal control system in practice. Therefore, sensitivity considerations are among the

fundamental aspects of the synthesis and analysis of optimal control systems.

One way to assess performance sensitivity is to substitute one by one the original values of the model parameters by slightly perturbed values and to compute the new optimal control and corresponding value of the performance criterion. This, however, is a rather time consuming procedure. In this research, a first-order approach to the sensitivity analysis of open-loop optimal control problems was used as derived by Courtin and Rootenberg (1971) and Evers (1979, 1980). Using variational arguments, the methodology requires a single calculation of the open-loop optimal control and corresponding state and costate trajectories. These are then used to calculate a first-order approximation of the performance sensitivity, thus saving a considerable amount of computation time.

Notation

c	model parameter	c_{V_T}	perturbation parameter on temperature outside greenhouse (1)
$c_{ai,ou}$	heat transmission coefficient through the greenhouse cover (6.1), $\text{W m}^{-2} \text{ } ^\circ\text{C}^{-1}$	$c_{\alpha\beta}$	yield factor (0.544)
$c_{cap,c}$	volumetric capacity of greenhouse air for carbon dioxide (4.1), $\text{m}^3 \text{ kg}^{-1}$	c_σ	weighting factor in penalty function, $\text{Hfl m}^{-2} \text{ s}^{-1}$
$c_{cap,h}$	volumetric capacity of greenhouse air for humidity (4.1), $\text{m}^3 \text{ kg}^{-1}$	c_Γ	carbon dioxide compensation point (5.2×10^{-5}), kg m^{-3}
$c_{cap,q}$	heat capacity of greenhouse air (30000), $\text{J m}^{-2} \text{ } ^\circ\text{C}^{-1}$	H	Hamiltonian, $\text{Hfl m}^{-2} \text{ s}^{-1}$
$c_{cap,q,v}$	heat capacity per volume unit of greenhouse air (1290), $\text{J m}^{-3} \text{ } ^\circ\text{C}^{-1}$	J	performance measure, Hfl m^{-2}
c_{co_2}	costs of carbon dioxide (42×10^{-2}), Hfl kg^{-1}	m	number of model parameters
$c_{co_2,1}$	temperature effect on CO_2 diffusion in leaves (5.11×10^{-6}), $\text{m s}^{-1} \text{ } ^\circ\text{C}^{-2}$	n	number of state variables
$c_{co_2,2}$	temperature effect on CO_2 diffusion in leaves (2.30×10^{-4}), $\text{m s}^{-1} \text{ } ^\circ\text{C}^{-1}$	i, j, k	iteration numbers
$c_{co_2,3}$	temperature effect on CO_2 diffusion in leaves (6.29×10^{-4}), m s^{-1}	p	penalty
c_{leak}	leakage air exchange through greenhouse cover (0.75×10^{-4}), m s^{-1}	p_T	penalty for constraint violations by greenhouse air temperature, $\text{Hfl m}^{-2} \text{ s}^{-1}$
$c_{pl,d}$	effective canopy surface (53), $\text{m}^2 \text{ kg}^{-1}$	p_c	penalty for constraint violations by carbon dioxide concentration, $\text{Hfl m}^{-2} \text{ s}^{-1}$
$c_{pri,1}$	parameter defining price of lettuce (1.8), Hfl m^{-2}	p_h	penalty for constraint violations by humidity, $\text{Hfl m}^{-2} \text{ s}^{-1}$
$c_{pri,2}$	parameter defining price of lettuce (16), Hfl kg^{-1}	$Q_{vent,q}$	energy exchange by ventilation and transmission through the cover, W m^{-2}
c_q	price of heating energy (6.35×10^{-9}), Hfl J^{-1}	$Q_{rad,q}$	heat load by solar radiation, W m^{-2}
c_R	gas constant (8314), $\text{J K}^{-1} \text{ kmol}^{-1}$	R_{Xh}	relative humidity
$c_{rad,phot}$	light use efficiency (3.55×10^{-9}), kg J^{-1}	t	time
$c_{rad,q}$	heat load coefficient due to solar radiation (0.2)	t_b	start time of optimisation interval
$c_{resp,d}$	respiration rate in terms of respired dry matter (2.65×10^{-7}), s^{-1}	t_f	end time of optimisation interval
$c_{resp,c}$	respiration rate in terms of produced carbon dioxide (4.87×10^{-7}), s^{-1}	u	control input
$c_{T,abs}$	temperature in K at 0°C (273.15), K	U_c	supply rate of carbon dioxide, $\text{kg m}^{-2} \text{ s}^{-1}$
$c_{v,pl,ai}$	canopy transpiration mass transfer coefficient (3.6×10^{-3}), m s^{-1}	U_q	energy supply by the heating system, W m^{-2}
$c_{v,1}$	parameter defining saturation water vapour pressure (9348), J m^{-3}	U_v	ventilation rate, m s^{-1}
$c_{v,2}$	parameter defining saturation water vapour pressure (17.4)	V_c	carbon dioxide concentration outside the greenhouse, kg m^{-3}
$c_{v,3}$	parameter defining saturation water vapour pressure (239), $^\circ\text{C}$	V_h	outdoor humidity concentration, kg m^{-3}
$c_{v,4}$	parameter defining saturation water vapour pressure (10998), J m^{-3}	V_{rad}	solar radiation outside the greenhouse, W m^{-2}
c_{V_c}	perturbation parameter on carbon dioxide concentration outside greenhouse (1)	V_T	outdoor temperature, $^\circ\text{C}$
$c_{V_{rad}}$	perturbation parameter on solar radiation outside greenhouse (1)	x	state variable
c_{V_h}	perturbation parameter on humidity outside greenhouse (1)	X_c	carbon dioxide concentration in greenhouse, kg m^{-3}
		X_d	crop dry weight, kg m^{-2}
		X_h	humidity concentration in greenhouse, kg m^{-3}
		X_T	air temperature in the greenhouse, $^\circ\text{C}$
		λ	costate
		λ_d	costate of crop dry weight, Hfl kg^{-1}
		λ_c	costate of carbon dioxide concentration, Hfl m kg^{-1}
		λ_h	costate of humidity concentration, Hfl m kg^{-1}
		λ_T	costate of air temperature, $\text{Hfl m}^{-2} \text{ } ^\circ\text{C}^{-1}$
		$\varphi_{phot,c}$	gross canopy photosynthesis rate, $\text{kg m}^{-2} \text{ s}^{-1}$
		$\varphi_{vent,c}$	mass exchange of carbon dioxide through the vents, $\text{kg m}^{-2} \text{ s}^{-1}$

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