



Design and optimization of solid thermal energy storage modules for solar thermal power plant applications



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HIGHLIGHTS

- An initial model is developed for a solid cylindrical heat storage unit.
- The analytical solution of the model is determined by using Laplace transform method.
- A new optimization method for the solid storage module design is proposed.
- The influence of design parameters on the storage cost is investigated.
- The optimization designs for various kinds of system requirement are studied.

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ABSTRACT

Solid sensible heat storage is an attractive option for high-temperature storage applications in terms of investment and maintenance costs. Typical solid thermal energy storage systems use a heat transfer fluid to exchange heat as the fluid flows through a tubular heat exchanger embedded in the solid storage material. The modified lumped capacitance method is used with an effective heat transfer coefficient in a simplified analysis of the heat transfer in solid thermal energy storage systems for a solid cylindrical heat storage unit. The analytical solution was found using the Laplace transform method. The solution was then used to develop an optimization method for designing solid storage modules which uses the system requirements (released energy and fluid outlet temperature) as the constraint conditions and the storage module cost as the objective function for the optimization. Optimized results are then given for many kinds of system configurations.

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1. Introduction

Power generation using concentrated solar thermal energy is one of several promising renewable energy technologies with a great amount of worldwide research devoted to the development of concentrated solar energy systems in the last ten years [1,2]. Thermal energy storage (TES) is essential for concentrating solar power (CSP) plant applications. The main advantages of integrating a CSP system with thermal storage include extended utilization of the power block and life expectancy of components due to the reduction of thermal transients [3–5]. Therefore, TES systems give CSP plants an edge over photovoltaics or wind power [6].

There are three kinds of TES including sensible heat storage (SHS), latent heat storage (LHS) and thermo-chemical heat storage

(TCHS) that uses reversible endothermic chemical reactions. LHS is based on the change of state of a material. The thermal energy is stored when the material changes state as the heat of fusion or heat of vaporization. Presently, the development of phase change material and design of the LHS systems have been widely investigated [7–11]. SHS uses solid or liquid media and involves storing energy in a material without phase change in the temperature range of the storage process. This technology is the most mature and has been widely used in CSP systems. Currently, the two-tank molten salt storage system with a high-temperature tank and a low-temperature tank for storing the molten salt is the most mature utility-scale TES system for CSP plants. Such systems have been applied in parabolic trough power plants including Andasol (1–3) in Spain, Archimede in Italy [12,13] and the power tower plant Gemasolar in Spain [14]. However, the disadvantages of this design are the very high cost of the material used as heat transfer fluid (HTF) and storage material, the high cost of the heat

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Nomenclature

| | | | |
|----------------|-----------------------------------------------------------------------------------------|----------------------|----------------------------------------------------------------|
| a | inner radius of the cylindrical heat storage unit (m) | S_i | insulation area (m ²) |
| b | outer radius of the cylindrical heat storage unit (m) | S_s | solid material section area (m ²) |
| C | specific heat (J/(kg K)) | T | temperature (°C) |
| d_h | tube wall thickness (m) | T_{amb} | ambient temperature (°C) |
| d_i | inner diameter of the heat storage unit (m) | $T_{f,allow}$ | allowed lowest fluid temperature (°C) |
| d_m | inner diameter of the main pipe (m) | T_{fin} | inlet fluid temperature (°C) |
| d_o | outer diameter of the heat storage unit (m) | T_{fout} | outlet fluid temperature (°C) |
| f | Darcy friction factor | T_H | initial storage unit temperature (°C) |
| h_E | corrected heat transfer coefficient (W/(m ² K)) | T_L | fluid inlet temperature (°C) |
| h | heat transfer coefficient (W/(m ² K)) | \bar{T}_f | mean fluid temperature (°C) |
| k_s | solid material thermal conductivity (W/m K) | \bar{T}_s | mean solid temperature (°C) |
| L | heat storage unit length (m) | $\bar{T}_{s,end}$ | mean solid temperature at the end of the discharge period (°C) |
| \dot{m} | mass flow rate (kg/s) | ΔT | difference between T_H and T_L (°C) |
| m_s | storage unit solid mass (kg) | t | time (s) |
| N | number of heat transfer tubes | t^* | dimensionless time |
| P | heat transfer surface perimeter of the cylindrical surface (m) | t_{dis} | discharge time (h) |
| P_{pump} | pump power (kW) | $t_{s,life}$ | storage module life (year) |
| p_i | total head loss (Pa) | $t_{p,life}$ | pump life (year) |
| $p_{l,main}$ | head loss in the main pipe (Pa) | U | average fluid velocity in the heat transfer tube (m/s) |
| $p_{l,branch}$ | head loss in the heat transfer tube (Pa) | U_m | average velocity in the main pipe (m/s) |
| p_m | local resistance loss (Pa) | \dot{V}_f | fluid volume flow (m ³ /h) |
| Δp | pressure drop (Pa) | | |
| Q_{dis} | energy obtained by the fluid (kW h) | | |
| Q_L | heat loss from storage module (kW h) | Greek symbols | |
| Q_{max} | maximum released energy from the storage module (kW h) | \mathcal{A} | Laplace transform of temperature |
| Q_s | released energy from storage unit (kW h) | σ | allowed lowest dimensionless fluid temperature |
| Q_{total} | effective energy released from the storage module during the entire storage module life | θ | dimensionless temperature |
| q_L' | heat loss flux (kW/m ²) | ρ | density (kg/m ³) |
| R_c | total concrete material cost (\$) | ζ | local friction factor |
| R_e | total cost of electricity for the pump (\$) | η | diameter ratio |
| R_i | total insulation material cost (\$) | | |
| $R_{material}$ | total material cost (\$) | Subscripts | |
| R_p | total pump cost (\$) | f | heat transfer fluid |
| R_s | total cost of heat transfer tube material (\$) | s | solid storage material |
| R_{total} | total storage module cost (\$) | | |
| r_c | heat transfer tube material cost per unit mass (\$/kg) | Acronym | |
| r_e | electricity cost per kW h (\$/kW h) | CSP | concentrating solar power |
| r_i | insulation material cost per unit area (\$/m ²) | FEM | finite element method |
| $r_{material}$ | material cost per unit storage capacity (\$/kW h) | HTF | heat transfer fluid |
| r_p | cost of one pump (\$) | GA | genetic algorithm |
| r_s | heat transfer tube material cost per unit mass (\$/kg) | LHS | latent heat storage |
| r_{total} | unit storage cost (\$/kW h) | SHS | sensible heat storage |
| s | Laplace transform parameter | SQP | sequential quadratic programming |
| S_f | wetted area in the tube (m ²) | TCHS | thermo-chemical heat storage |
| | | TES | thermal energy storage |

exchangers, and the risk of solidification of the storage fluid because of its relatively high melting point which increases the maintenance and operating costs [15]. Solid sensible heat storage using concrete or ceramic as the storage material is expected to be an attractive option due to its lower investment and maintenance costs [16–18].

Concrete energy storage provides a regenerative storage system where the storage module is cyclically heated and cooled by the HTF. The fluid typically flow through a tubular heat exchanger with a defined tube pitch that is imbedded in the concrete [19]. The feasibility of such systems has already been proven in laboratory scale tests [20].

A large number of material tests such as thermal cycling and strength tests have been carried out by Laing et al. [6,19] and John et al. [21] to develop and optimize the mixture of the high-temper-

ature concrete material. Laing et al. [6] place graphite between the layers of precast concrete slabs to improve the heat transfer between the concrete and the heat changer tube. Finite element method (FEM) calculation results showed that this structure could reduce the number of tubes by 47%. Selvam et al. [22] investigated heat transfer within a passive system considering four kinds of fin configurations including rods, disks, plates, and spiral fins. Various fin thicknesses and spacing were considered for each fin configuration using 3D FEM models. Zhu et al. [23] added six graphite sheets around a smooth tube to enhance the heat transfer into the concrete storage unit. The results showed that the graphite sheets significantly increased the equivalent thermal conductivity of the concrete by 4.7 times.

The German Aerospace Center (DLR) successfully tested a concrete storage unit and a castable ceramic storage unit on the

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